# Synthesis, Characterization and Corrosive Inhibition Study of Phenylamino Cyclohexenone: Mild Steel Corrosion Studies in Acidic Medium

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#### Abstract

The present study reveals the greener synthesis and corrosion inhibition study of phenylamino cyclohex-2enone (PAC) derivatives. Microwave assisted synthesis is one of the safe and environmental friendly method to synthesize cyclohex-2-enone compounds in presence of sodium bisulphate used as a catalyst and it is a highly economical one. The cyclohex-2-enone compounds corrosion inhibitive effect proved with the help of its weight loss. Synergetic process, electro chemical impedence and potentiodynamic polarization studies was carried out for the target compounds.

The structures of synthesized cycloexenone compounds were elucidated with the help of IR, <sup>1</sup>H and <sup>13</sup>C NMR. The type of adsorption isotherm was confirmed by using synergetic process. The synergetic process was done by observing the correlation between halides and inhibitor. The final results show that the compounds follow the Langmuir adsorption isotherm.

**Keywords**: 5,5-dimethyl -3-(phenylamino)-cyclohex-2enone, Microwave irradiation, Adsorption isotherm, Kinetics, Synergetic effect.

### Introduction

The movement of electron between ionic current of the solution and electronic current in the metal causes the corrosion in the metal surface. Corrosion is an electrochemical process in nature. It occurred at oil pickling process pipes and other industrial pipe lines which are used to carry the acidic, basic solutions to internal processes. The acidification of a well increases its permeability but corrosion risks should also be considered<sup>16,18</sup>.

Inhibitors are chemical compounds which are used to control the corrosion effect on the pipe lines, metallic machines and other iron components. The use of inhibitor is one of the economic and common techniques to reduce the corrosion process in the pipes<sup>13,21</sup>.

The organic compounds have ability to control this corrosion process<sup>14</sup>. Mostly, active inhibitors contain hetero atoms like N, S, O in their skeleton structures<sup>3,4</sup>. The ability of the inhibitors has been observed by considering physic-chemical properties such as inhibitors functional group, electron density of donor atom, molecular size, pi-orbital

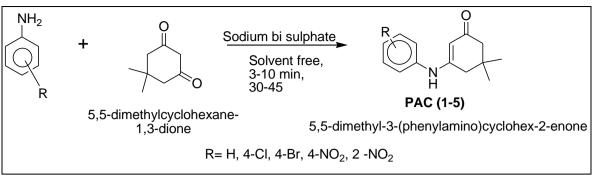
character and electronic structure<sup>1,9</sup>. The combination of chemical and electrochemical technique studies along with surface analytical techniques is very effective method to find out the active inhibitors<sup>1</sup>. Current studies proved that if the number of heteroatom increases in the inhibitor its corrosion inhibition property increases<sup>11</sup>. Good inhibition result was found from the inhibition study of Schiff bases at mild steel on acidic medium<sup>2,5,12</sup>. The skeleton structure of Schiff bases contains both hetero atom and pi-electron system which are most preferred one for adsorption property of a molecule. Inhibition efficiency always depends on active adsorption centres present in inhibitor molecule<sup>6</sup>. Present study reveals that the most of the organic compounds have effective inhibition property, the molecules pyridazine<sup>17</sup>, mercaptans, thioethers<sup>19</sup>, methionine methvl oximes. ester hydrochloride<sup>15</sup>, pyrazole<sup>7,8</sup> and alkyl esters<sup>6,10</sup>. The piperidone have an effective inhibitor property due to presence of C=O and NH- group<sup>2</sup>. Our newly synthesized PAC derivatives also have the same groups in its electronic structure. They stimulate present corrosion inhibition effect of PAC compounds on mild steel in the HCl and H<sub>2</sub>SO<sub>4</sub> environment. The compound inhibition efficiency have been evaluated with the help of electrochemical impedance and polarization values.

### **Material and Methods**

The metal strips which are used for corrosion studies contain  $3.15 \,\%$  of carbon, 0.61% of manganese,  $0.155 \,\%$  of chromium, 0.07% of phosphorus,  $0.049 \,\%$  of sulphur,  $0.035 \,\%$  of tin and remaining percentage is of iron<sup>11</sup>.

**Materials:** The triple distilled analytical grade water was used to prepare the acid solutions. 1M H<sub>2</sub>SO<sub>4</sub> and 1M HCl were used as corrosion medium. 10, 20, 30, 40 and 50 ml concentration inhibitors were employed for the studies. The experiments were performed as triplicate and the average value of the weight loss and electrochemical test were reported. The clean set of electrodes and freshly prepared solutions were used. The metallic rod for the weight loss tests have the dimension of 1cm x 5 cm x 0.33 cm and working electrodes have surface area about 0.339 cm<sup>2</sup>.

The electrode was first mechanically treated using various grades of grinding paper (up to 1200 grit) and then polished with the help of emery sheets with 1/0 to 4/0 grades to remove adhering impurities before every single corrosion test. Finally strips were cleaned by using double distilled water and ethanol.



Scheme 1: The microwave assisted pathway of phenylamino cyclohex-2-enones.

**Instruments:** The skeleton structure of the organic inhibitor was confirmed by using Perkin-Elmer 1650 spectrometer and Bruker AMX 400 NMR spectrometers. The Perkin-Elmer 1650 was used for IR studies with the absorption unit cm<sup>-1</sup>. Bruker AMX instrument was used to predict and carryout the <sup>1</sup>H and <sup>13</sup>C NMR values of the inhibitors with the unit ppm and the standard was TMS, CDCl<sub>3</sub> as solvent. The single-mode microwave reactor was used for synthesis purpose under control pressure, temperature and power. Maspec MSW 9629 spectrometer was used to obtain the mass spectra value of the inhibitor.

**Organic Inhibitor:** Organic inhibitor is a compound which reduces the corrosion effect of steel rod in acidic medium. It has a function either anodic or cathodic or both. Many of the organic compounds have to reduce the corrosion rate of the iron or steel rods in acidic medium. The inhibition activity was performed by additive adsorption between the metal-acid solution interfaces. This is known as potential difference of the interface. The changes occur in the size and properties of inhibitor at the interface due to formation of electrical double layer. The displacement reaction during adsorption process is written as:

 $Org_{(sol)} + nH_2O \longrightarrow Org_{(ads)} + nH_2O$ 

The number of removal of water molecules indicates the number of adsorbed inhibitors on metal surface. Adsorption of organic molecule occurs because the interaction energy is between the metal surface and inhibitor due to presence of ionization energy between them. Especially, there are three types of inhibition effect mode. (i) geometric blocking effect, (ii) blocking the active sites and (iii) electro-catalytic effect of the inhibitor or reaction products. In the first mode, inhibition occurs due to reduction of reaction and other modes occur due to change in activation energy barriers of the anodic or cathodic reaction. There is some deviation in electrochemical behaviour between interpreted and measured electrochemical data because there is presence of factors affecting inhibitors.

**Effect of temperature of organic compounds on metal:** Most of the organic inhibitors contain at least one polar group like N, S or Se, P in some cases. The inhibition properties of organic compounds were understood by the electron density of the reaction centre. The chemisorptions bond strengthened between metal surface and inhibitor with increases in electron density of the reaction centres in inhibitor. Electron density increases when unshared pair of electron in polar compounds is detached. The corrosion monitoring methods known as weight loss, electrochemical and potentiometric studies give adsorption details of inhibitor molecules. These tests are taken by using suitable method and instruments.

**Corrosion monitoring method- (i) Weight loss tests:** Weight loss measurements were performed at different temperatures  $(35^{\circ}, 45^{\circ}, 55^{\circ} \text{ and } 65^{\circ})$  of carbon steel under 20 ml of HCl and H<sub>2</sub>SO<sub>4</sub> medium and the same studies were also done by different inhibitor concentrations with 20 ml of acids at room temperature. The blank value was also noted for every reading. At the end of the test, the specimens were cleared and finally weight loss were recorded. The corrosion rate, inhibition efficiency and surface coverage were determined by following equations:

where W is weight loss (g), D is the density of steel (g cm<sup>-3</sup>), A is the surface area (cm<sup>2</sup>), T is the time in hours and  $V_{corr,0}$ ,  $V_{corr,i}$  are the weight loss values in the presence and absence of inhibitor.

**Electrochemical tests:** Electrochemical tests are mainly done by identify the kinetics of cathode and anode potentials in the electrode. The electrochemical tests were performed by using three electrode glass cells. 99.9% purity platinum electrode was considered as a counter electrode and the electrode was made up of mild steel (0.339cm<sup>2</sup>) used as a working electrode and its electrode potential was measured against a standard calomel electrode (SCE).

The setup of electrochemical instrument, method of working and calculation of polarization resistance values are followed as given in the previous studies<sup>11</sup>. The inhibition of efficiency of the organic inhibitor was measured from its polarization resistance value by using following formulas:

$$[(I.E)_{R_p,\%}] = \frac{R_p^i - R_p^0}{R_p^i} \times 100$$

$$\left[(I.E)_{T,}\%\right] = \frac{i_{corr}^0 - i_{corr}^i}{i_{corr}^0} \times 100$$

where  $R_p^0$  and  $R_p^i$  indicate the polarization resistance in the absence and presence of inhibitor respectively and  $i_{corr}^i$  and  $i_{corr}^0$  are the corrosion current density values in presence and absence of inhibitor. The corrosion densities ( $i_{corr}$ ) from the Tafel extraplotations was also used to determine the inhibition efficiency.

## **Results and Discussion**

**Structural confirmation of Organic Inhibitor:** The PAC target compounds were synthesized using Schiff reaction between substituted aniline and 5,5- dimethyl substituted cyclohexan-1,3-dione via microwave irradiation. Microwave method is one of the best and eco-friendly method to synthesise these type of organic inhibitors and is also time saving and economical method. The skeleton structures were confirmed by using elemental analysis spectral data are given as follows:

PAC-1 (5,5-dimethyl-3-(phenylamino)cyclohex-2-enone: Yield 70%, m.p. 100°C, Molecular Formula C<sub>14</sub>H<sub>17</sub>NO; %Calcd. (Found): C%= 51.42 (78.10). H% =4.28 (7.96). N% = 7.8 (6.51), O%=9.16 (7.43). M/z (M) +:215.3; FT-IR (KBr, cm<sup>-1</sup>): 3042.09 cm-1(Aromatic CH stretching), 2889.54cm<sup>-1</sup> (Aliphatic CH stretching), 1656.67 cm<sup>-</sup> <sup>1</sup>(Amide C=O stretching), 1418.05 cm<sup>-1</sup>(C=N Stretching), 645.15, 735.42, 784.42 cm<sup>-1</sup>(Aromatic ring stretching); <sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm, 400 MHz) 1.02-1.11 (m, 6H of CH<sub>3</sub>), 1.88-2.86 (m, 4H of methylene in cyclohexanone), 3.62 (S, 1H of NH), 5.54 (d, 1H of C-2 of cyclohexanone), 6.48-7.15(Aromatic protons); <sup>13</sup>C NMR (CDCl<sub>3</sub>, δ ppm,100 MHz): 198.93 (C=O). 27.21 (methvl group in cyclohexanone ring), 99.08 (C-2 of cyclohexanone), 162.35 (C-3 of cyclohexanone), 43.08 (C-4 of cyclohexanone), 31.59 (C-5 of cyclohexanone), 52.73 (C-6 of cyclohexanone),122.56-144.08 (Aromatic carbons).

PAC-2 (5,5-dimethyl-3-(4-chlorophenylamino)cyclohex-2-enone: Yield 70%, m.p. 100°C, Molecular Formula C<sub>14</sub>H<sub>16</sub>NOCl; %Calcd. (Found); C%= 51.42 (67.33), H% =4.28 (6.46), N% = 7.8 (5.61) O%=9.16 (6.41), Cl% = (14.20). M/z (M) +:249.09; FT-IR (KBr, cm<sup>-1</sup>): 3076.23 cm<sup>-1</sup> <sup>1</sup>(Aromatic CH stretching), 2888.45cm<sup>-1</sup> (Aliphatic CH stretching), 1652.25 cm<sup>-1</sup>(Amide C=O stretching), 1412.51 cm<sup>-1</sup>(C=N Stretching), 654.15, 710.54, 783.91 cm<sup>-1</sup> <sup>1</sup>(Aromatic ring stretching); <sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm, 400 MHz) 1.03-1.25 (m, 6H of CH<sub>3</sub>), 2.14-2.84 (m, 4H of methylene in cyclohexanone), 3.62 (S, 1H of NH), 5.68 (d, 1H of C-2 of cyclohexanone), 6.45-7.87(Aromatic protons); <sup>13</sup>C NMR (CDCl<sub>3</sub>, δ ppm,100 MHz): 198.82 (C=O), 28.42 (methyl group in cyclohexanone ring), 97.43 (C-2 of cyclohexanone), 162.14 (C-3 of cyclohexanone), 43.48 (C-4 of cyclohexanone), 32.95 (C-5 of cyclohexanone), 51.25 (C-6 of cyclohexanone),117.71-142.53 (Aromatic carbons).

PAC-3 (5,5-dimethyl-3-(4-bromophenylamino)cyclohex-2-enone: Yield 70%, m.p. 100°C, Molecular Formula C<sub>14</sub>H<sub>16</sub>NOBr; %Calcd. (Found); C%= 51.42 (57.16), H% =4.28 (5.48), N% = 7.8 (4.76) O%=9.16 (5.44), Br%= (27.16). M/z (M) +:350,352; FT-IR (KBr, cm<sup>-1</sup>): 3066.11 cm<sup>-1</sup>(Aromatic CH stretching), 2885.51cm<sup>-1</sup> (Aliphatic CH stretching), 1658.78 cm<sup>-1</sup>(Amide C=O stretching), 1417.68 cm<sup>-1</sup>(C=N Stretching), 642.3, 709.8, 763.81 cm<sup>-1</sup>(Aromatic ring stretching); <sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm, 400 MHz) 1.06-1.48 (m, 6H of CH<sub>3</sub>), 2.18-2.58 (m, 4H of methylene in cyclohexanone), 3.12 (S, 1H of NH), 5.76 (d, 1H of C-2 of cyclohexanone), 6.97-7.53(Aromatic protons); <sup>13</sup>C NMR ( CDCl<sub>3</sub>, δ ppm,100 MHz): 198.52 (C=O), 28.61 (methyl cyclohexanone ring), 97.56 (C-2 of group in cyclohexanone), 162.84 (C-3 of cyclohexanone), 43.38 (C-4 of cyclohexanone), 33.09 (C-5 of cyclohexanone), 50.73 (C-6 of cyclohexanone),124.28-138.93 (Aromatic carbons).

PAC-4 (5,5-dimethyl-3-(4-nitrophenylamino)cyclohex-2enone: Yield 70%, m.p. 100°C, Molecular Formula  $C_{14}H_{16}N_2O_3$ ; %Calcd. (Found); C%= 64.42 (64.60), H% =4.28 (6.20), N% = 7.8 (10.76) O%=9.16 (18.44). M/z (M) +: 260.12; FT-IR (KBr, cm<sup>-1</sup>): 3065.23 cm<sup>-1</sup>(Aromatic CH stretching), 2881.74cm<sup>-1</sup> (Aliphatic CH stretching), 1657.15 cm<sup>-1</sup>(Amide C=O stretching), 1417.88 cm<sup>-1</sup>(C=N Stretching), 652.30, 712.57, 788.99 cm<sup>-1</sup>(Aromatic ring stretching); <sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm, 400 MHz) 1.04-1.50 (m, 6H of CH<sub>3</sub>), 2.14-2.64 (m, 4H of methylene in cyclohexanone), 3.09 (S, 1H of NH), 5.48 (d, 1H of C-2 of cyclohexanone), 6.72-7.94 (Aromatic protons); <sup>13</sup>C NMR ( CDCl<sub>3</sub>, δ ppm,100 MHz): 198.95 (C=O), 29.05 (methyl (C-2 group in cyclohexanone ring), 98.18 of cyclohexanone), 162.23 (C-3 of cyclohexanone), 43.14 (C-4 of cyclohexanone), 32.89 (C-5 of cyclohexanone), 50.83 (C-6 of cyclohexanone), 121.92-146.88 (Aromatic carbons).

PAC-5 (5,5-dimethyl-3-(2-nitrophenylamino)cyclohex-2enone: Yield 70%, m.p. 100°C, Molecular Formula C<sub>14</sub>H<sub>16</sub>N<sub>2</sub>O<sub>3</sub>; %Calcd. (Found); C%= 51.42 (64.60), H% =4.28 (6.20), N% = 7.8 (10.76) O%=9.16 (18.44); FT-IR (KBr, cm<sup>-1</sup>): 3065.47 cm<sup>-1</sup>(Aromatic CH stretching), 2882.12 cm<sup>-1</sup> (Aliphatic CH stretching), 1657.85 cm<sup>-</sup> <sup>1</sup>(Amide C=O stretching), 1417.56 cm<sup>-1</sup>(C=N Stretching), 653.03, 713.61, 785.96 cm<sup>-1</sup>(Aromatic ring stretching); <sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm, 400 MHz) 1.05-1.56 (m, 6H of CH<sub>3</sub>), 2.09-2.46 (m, 4H of methylene in cyclohexanone), 3.11 (S, 1H of NH), 5.45 (d, 1H of C-2 of cyclohexanone), 6.74-7.96 (Aromatic protons); <sup>13</sup>C NMR (CDCl<sub>3</sub>, δ ppm, 100 MHz): 198.91 (C=O), 29.12 (methyl group in cyclohexanone ring), 98.16 (C-2 of cyclohexanone), 162.24 (C-3 of cyclohexanone), 43.18 (C-4 of cyclohexanone), 32.91 (C-5 of cyclohexanone), 50.85 (C-6 of cyclohexanone),121.98-145.93 (Aromatic carbons).

From the above data, carbon structures of the organic inhibitors (PAC 1-5) were confirmed and the common structure is shown in figure 1.

Weight loss measurement: The inhibition efficiency with different concentrations of the inhibitor PAC on the mild

steel in  $1M H_2SO_4$  and 1M HCl has been evaluated by weight loss measurements and the results are summarized in table 1.

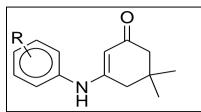


Figure 1: The common structure of PAC inhibitors

The data reveals that inhibition efficiency increases with increase in concentration of the inhibitors. The behavior may be attributed to an increase in surface coverage ( $\theta$ ) by the adsorption of inhibitor on the mild steel surface, in the aggressive solution which restricts the dissolution of the metal.

**Effect of temperature:** The effect of temperature on the inhibited acid-metal reaction is highly complex because many changes occur on the metal surface such as rapid etchings, desorption of the inhibitor and the inhibitor may undergo decomposition and/ or rearrangement. To evaluate

the effect of temperature on the adsorption behaviour as well as to determine the activation parameters of the corrosion of mild steel in  $1M H_2SO_4$  solution and  $1M H_2SO_4$  solution containing the inhibitors, the weight loss measurements were carried out in the temperature range of (301-318K) and the results are presented in table 2.

The data reveals that as the temperature is increased, the corrosion rate increased and the inhibition efficiency decreased. The decrease in the inhibition efficiency with increase in temperature may be attributed to the increase in the solubility of the protective film or the reaction products precipitated on the surface of the metal that might otherwise inhibit the reaction. This is in accordance with Ergun et al<sup>10</sup>.

The corrosion rate (CR) of the mild steel in acidic media is related to the temperature by the Arrhenius equation:

Log CR = log A - Ea/ 2.303 RT

where CR is the corrosion rate, Ea is the apparent activation energy, R is the molar gas constant, T is the absolute temperature and A is the frequency factor. The plot of log CR vs 1/T is shown in fig. 2. Linear plots were obtained.

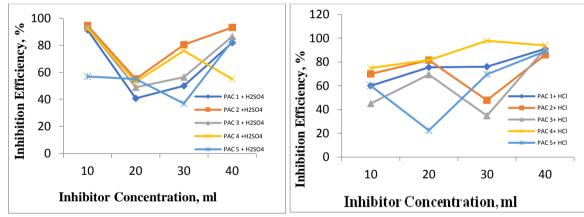


Figure 2: (a) plot of inhibition concentration against inhibition efficiency of mild steel in IM H<sub>2</sub>SO<sub>4</sub> of inhibitor PAC (1-5), (b) plot of inhibition concentration against inhibition efficiency of mild steel in IM HCl of inhibitor PAC (1-5).

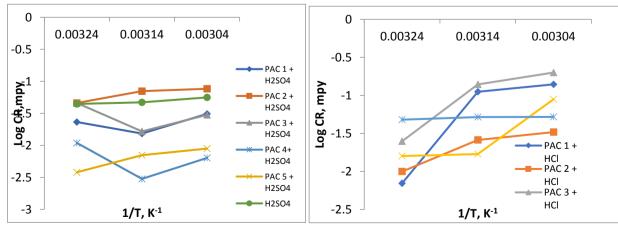


Figure 3: (a) plot of inhibition concentration against inhibition efficiency of mild steel in IM H<sub>2</sub>SO<sub>4</sub> of inhibitor PAC (1-5), (b) plot of inhibition concentration against inhibition efficiency of mild steel in IM HCl of inhibitor PAC (1-5).

| of 1M HCl and H <sub>2</sub> SO <sub>4</sub>   |             |                 |               |        |                      |  |  |  |  |
|--|-------------|-----------------|---------------|--------|----------------------|--|--|--|--|
| Inhibitor  | Weight loss | Inhibition      | Degree of     | C/0    | Corrosion            |  |  |  |  |
| concentration in %   | in mg       | Efficiency in % | coverage in θ |        | rate in              |  |  |  |  |
|  |             |                 |               |        | mpy*10 <sup>-3</sup> |  |  |  |  |
| Blank (10 ml)  | 0.093       | -               |               | _      | 0.0478               |  |  |  |  |
| $H_2SO_4+PAC 1$  | 0.008       | 91.39           | 0.91          | 10.989 | 0.368                |  |  |  |  |
| $H_2SO_4 + PAC 2$  | 0.005       | 94.62           | 0.94          | 21.276 | 0.832                |  |  |  |  |
| $\frac{H_2SO_4 + PAC 2}{H_2SO_4 + PAC 3}$  | 0.005       | 93.54           | 0.93          | 32.258 | 0.999                |  |  |  |  |
| $\frac{H_2SO_4 + PAC S}{H_2SO_4 + PAC 4}$  | 0.007       | 92.47           | 0.92          | 43.478 | 1.165                |  |  |  |  |
| $\frac{H_2SO_4 + PAC}{H_2SO_4 + PAC}$  | 0.005       | 56.98           | 0.92          | 53.191 | 0.832                |  |  |  |  |
| Blank (20 ml)  | 0.049       | -               | -             | -      | 0.0251               |  |  |  |  |
| $H_2SO_4+PAC 1$  | 0.029       | 40.81           | 0.40          | 50     | 0.088                |  |  |  |  |
| $H_2SO_4 + PAC 2$  | 0.022       | 55.10           | 0.55          | 36.36  | 0.028                |  |  |  |  |
| $\frac{H_2SO_4 + PAC 2}{H_2SO_4 + PAC 3}$  | 0.073       | 48.97           | 0.48          | 41.66  | 0.093                |  |  |  |  |
| $\frac{H_2SO_4 + PAC 3}{H_2SO_4 + PAC 4}$  | 0.023       | 53.06           | 0.53          | 37.73  | 0.029                |  |  |  |  |
| $H_2SO_4 + PAC + FAC $ | 0.022       | 55.10           | 0.55          | 36.36  | 0.029                |  |  |  |  |
| $\frac{112504 + 1 \text{ AC } 5}{\text{Blank (30 ml)}}$  | 0.022       | -               | -             | -      | 0.023                |  |  |  |  |
| $H_2SO_4+PAC 1$  | 0.069       | 50              | 0.50          | 60     | 0.088                |  |  |  |  |
| $\frac{H_2SO_4 + PAC T}{H_2SO_4 + PAC T}$  | 0.009       | 80.43           | 0.80          | 37.5   | 0.011                |  |  |  |  |
| $\frac{H_2SO_4 + PAC 2}{H_2SO_4 + PAC 3}$  | 0.000       | 56.52           | 0.56          | 53.57  | 0.025                |  |  |  |  |
| $\frac{H_2SO_4 + PAC 3}{H_2SO_4 + PAC 4}$  | 0.020       | 76.08           | 0.76          | 39.47  | 0.023                |  |  |  |  |
| $\frac{H_2SO_4 + PAC 4}{H_2SO_4 + PAC 5}$  | 0.029       | 36.95           | 0.36          | 83.33  | 0.014                |  |  |  |  |
| $\frac{1}{1}$ Blank (40 ml)  | 0.029       | 30.93           | 0.50          | 65.55  | 0.037                |  |  |  |  |
| $H_2SO_4 + PAC 1$  | 0.089       | 82.02           | 0.82          | 48.78  | 2.664                |  |  |  |  |
|  | 0.016       | 93.25           | 0.82          | 43.01  | 10.825               |  |  |  |  |
| $H_2SO_4 + PAC 2$  | 0.008       | 86.51           | 0.93          |        |                      |  |  |  |  |
| $H_2SO_4 + PAC 3$  |             |                 |               | 45.97  | 1.998                |  |  |  |  |
| $H_2SO_4 + PAC 4$  | 0.040       | 55.05           | 0.55          | 72.72  | 6.662                |  |  |  |  |
| $H_2SO_4+PAC 5$  | 0.015       | 83.14           | 0.83          | 48.19  | 2.498                |  |  |  |  |
| Blank (10 ml)  | 0.02        | -               | -             | -      | 0.1027               |  |  |  |  |
| HCl+ PAC 1   | 0.008       | 60              | 0.60          | 16.666 | 1.332                |  |  |  |  |
| HCl + PAC 2  | 0.006       | 70              | 0.7           | 28.571 | 0.999                |  |  |  |  |
| HCl + PAC 3  | 0.011       | 45              | 0.45          | 66.66  | 1.832                |  |  |  |  |
| HCl + PAC 4  | 0.005       | 75              | 0.75          | 53.331 | 0.832                |  |  |  |  |
| HCl + PAC 5  | 0.008       | 60              | 0.60          | 83.33  | 1.332                |  |  |  |  |
| Blank (20 ml)  | 0.049       | -               | -             | -      | 0.0096               |  |  |  |  |
| HCl+ PAC 1   | 0.012       | 75.51           | 0.75          | 26.66  | 0.015                |  |  |  |  |
| HCl + PAC 2  | 0.009       | 81.63           | 0.81          | 24.69  | 0.014                |  |  |  |  |
| HCl + PAC 3  | 0.015       | 69.38           | 0.69          | 28.98  | 0.019                |  |  |  |  |
| HCl + PAC 4  | 0.009       | 81.63           | 0.81          | 24.69  | 0.011                |  |  |  |  |
| HCl + PAC 5  | 0.060       | 22.44           | 0.22          | 90.90  | 0.076                |  |  |  |  |
| Blank (30 ml)  | 0.046       | -               | -             | -      | 0.012                |  |  |  |  |
| HCl+ PAC 1   | 0.011       | 76.0            | 0.76          | 39.47  | 0.014                |  |  |  |  |
| HCl + PAC 2  | 0.024       | 47.8            | 0.47          | 63.82  | 0.030                |  |  |  |  |
| HCl + PAC 3  | 0.03        | 34.78           | 0.35          | 85.71  | 0.070                |  |  |  |  |
| HCl + PAC 4  | 0.001       | 97.82           | 0.97          | 30.92  | 0.012                |  |  |  |  |
| HCl + PAC 5  | 0.013       | 69.56           | 0.69          | 43.47  | 0.016                |  |  |  |  |
| Blank (40 ml)  | 0.058       | -               | -             | -      | 0.298                |  |  |  |  |
| HCl+ PAC 1   | 0.005       | 91              | 0.91          | 43.95  | 0.832                |  |  |  |  |
| HCl + PAC 2  | 0.008       | 86              | 0.86          | 46.511 | 1.332                |  |  |  |  |
| HCl + PAC 3  | 0.005       | 91              | 0.91          | 43.95  | 0.832                |  |  |  |  |
| HCl + PAC 4  | 0.003       | 94              | 0.94          | 42.55  | 0.4979               |  |  |  |  |
| HCl + PAC 5  | 0.006       | 89              | 0.89          | 44.94  | 0.9958               |  |  |  |  |

 Table 1

 Inhibition efficiency of PAC inhibitors at various concentration immersed at various concentrations of 1M HCl and H<sub>2</sub>SO<sub>4</sub>

| hibition efficiency of PAC (1-5) inhibitors at various temperature 35°C, 45°C and 55°C of 1M HCl andInhibitorWeight lossInhibition EfficiencyDegree ofCorroside |        |       |                            |        |                          |  |  |
|---|--------|-------|----------------------------|--------|--------------------------|--|--|
| concentration in %  | in mg  | in %  | Degree of<br>coverage in θ | C/θ    | Corrosion<br>rate in Mpy |  |  |
|   | 0      |       | coverage in o              | C/0    |                          |  |  |
| $\frac{\text{Blank} (35^{\circ}\text{C})}{\text{U SO} + \text{DAC 1}}$  | 0.034  | - 55  | 0.55                       | -      | 0.0443 0.0231            |  |  |
| $H_2SO_4 + PAC 1$   | 0.018  |       |                            | 1.8181 |                          |  |  |
| $H_2SO_4 + PAC 2$   | 0.036  | 10    | 0.10                       | 10     | 0.0459                   |  |  |
| $H_2SO_4 + PAC 3$   | 0.036  | 10    | 0.10                       | 10     | 0.0459                   |  |  |
| H <sub>2</sub> SO <sub>4</sub> + PAC 4  | 0.0038 | 90.5  | 0.90                       | 1.111  | 1.0048                   |  |  |
| $H_2SO_4 + PAC 5$   | 0.003  | 92.5  | 0.92                       | 1.086  | 0.0038                   |  |  |
| Blank (45°C)  | 0.036  | -     | -                          | -      | 0.047                    |  |  |
| H <sub>2</sub> SO <sub>4</sub> + PAC 1  | 0.012  | 67.73 | 0.67                       | 1.492  | 0.0153                   |  |  |
| $H_2SO_4 + PAC 2$   | 0.06   | 62.16 | 0.62                       | 1.6129 | 0.0765                   |  |  |
| $H_2SO_4 + PAC 3$   | 0.013  | 64.86 | 0.64                       | 1.562  | 0.0165                   |  |  |
| $H_2SO_4 + PAC 4$   | 0.050  | 35.13 | 0.35                       | 2.857  | 0.0638                   |  |  |
| $H_2SO_4 + PAC 5$   | 0.007  | 81.08 | 0.81                       | 1.234  | 0.0089                   |  |  |
| Blank (55°C)  | 0.043  | -     | -                          | -      | 0.0561                   |  |  |
| H <sub>2</sub> SO <sub>4</sub> + PAC 1  | 0.025  | 41.86 | 0.41                       | 2.439  | 0.031                    |  |  |
| $H_2SO_4 + PAC 2$   | 0.055  | 27.90 | 0.27                       | 3.703  | 0.070                    |  |  |
| $H_2SO_4 + PAC 3$   | 0.024  | 44.18 | 0.44                       | 2.272  | 0.030                    |  |  |
| H <sub>2</sub> SO <sub>4</sub> + PAC 4  | 0.003  | 93.02 | 0.93                       | 1.075  | 0.003                    |  |  |
| $H_2SO_4 + PAC 5$   | 0.006  | 86.04 | 0.86                       | 1.162  | 0.007                    |  |  |
| Blank (35°C)  | 0.04   | -     | -                          | -      | 0.052                    |  |  |
| HCl+ PAC 1  | 0.006  | 85.0  | 0.85                       | 1.176  | 0.007                    |  |  |
| HCl + PAC 2   | 0.008  | 80.0  | 0.80                       | 1.250  | 0.010                    |  |  |
| HCl + PAC 3   | 0.011  | 72.5  | 0.72                       | 1.388  | 0.140                    |  |  |
| HCl + PAC 4   | 0.010  | 75    | 0.75                       | 1.333  | 0.012                    |  |  |
| HCl + PAC 5   | 0.013  | 168.7 | 0.168                      | 5.952  | 0.016                    |  |  |
| Blank (45°C)  | 0.037  | -     | -                          | -      | 0.048                    |  |  |
| HCl+ PAC 1  | 0.011  | 70.27 | 0.70                       | 1.428  | 0.140                    |  |  |
| HCl + PAC 2   | 0.021  | 43.24 | 0.43                       | 2.325  | 0.026                    |  |  |
| HCl + PAC 3   | 0.002  | 94.59 | 0.94                       | 1.063  | 0.025                    |  |  |
| HCl + PAC 4   | 0.004  | 89.18 | 0.89                       | 1.123  | 0.051                    |  |  |
| HCl + PAC 5   | 0.014  | 62.16 | 0.62                       | 1,612  | 0.017                    |  |  |
| Blank (55°C)  | 0.040  | -     | -                          | -      | 0.0087                   |  |  |
| HCl+ PAC 1  | 0.006  | 85.0  | 0.85                       | 1.176  | 0.007                    |  |  |
| HCl + PAC 2   | 0.003  | 92.0  | 0.92                       | 1.086  | 0.003                    |  |  |
| HCl + PAC 3   | 0.157  | 292.5 | 0.292                      | 3.424  | 0.200                    |  |  |
| HCl + PAC 4   | 0.009  | 77.5  | 0.272                      | 1.298  | 1.011                    |  |  |
| HCl + PAC 5   | 0.007  | 82.5  | 0.82                       | 1.219  | 0.089                    |  |  |



In **D**4

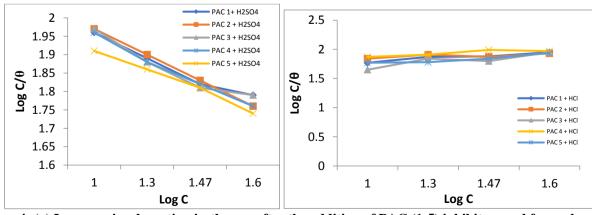


Figure 4: (a) Langumuir adsorption isotherms after the addition of PAC (1-5) inhibitor used for carbon steel in IM H<sub>2</sub>SO<sub>4</sub>, (b) Langumuir adsorption isotherms after the addition of PAC (1-5) inhibitor used for carbon steel in IM HCl.

Adsorption isotherm: Adsorption of the inhibitor molecules mainly depends on the charge and nature of the metal surface, electronic characteristics of the metal surface, temperature, adsorption of the solvent, ionic species and the electrochemical potential at the solution interface. The adsorption isotherm describes the adsorption behaviour of organic compounds. The most frequently used adsorption isotherms are Langmuir, Tempkin, Frumkin and Freundlich. To obtain the adsorption isotherm, the degree of surface coverage ( $\theta$ ) was calculated for various concentrations of PAC inhibitors from the weight loss data listed in table 1.

Adsorption behaviour of PAC inhibitors is best explained by Langmuir adsorption isotherm. Langmuir isotherm is an ideal isotherm for physical or chemical adsorption where there is no interaction between the adsorbate and adsorbent <sup>11</sup>. Assumption of Langmuir relates the concentration of the adsorbate in the bulk of the electrolyte (C) to the degree of surface coverage ( $\theta$ ) according to the equation:

 $C/\theta = 1/K + C$ 

where 'K' is the equilibrium constant of adsorption.

Applicability of Langmuir adsorption isotherm to the adsorption of PAC inhibitors on mild steel confirms the formation of multimolecular layer of adsorption where there is no interaction between the adsorbate and the adsorbent.

**Potentiometric polarization tests:** In iron or steel corrosion, electrochemical reactions may take place as follows:

At the anodic areas:

Fe  $\longrightarrow$  Fe<sup>2+</sup> + 2e<sup>-</sup>

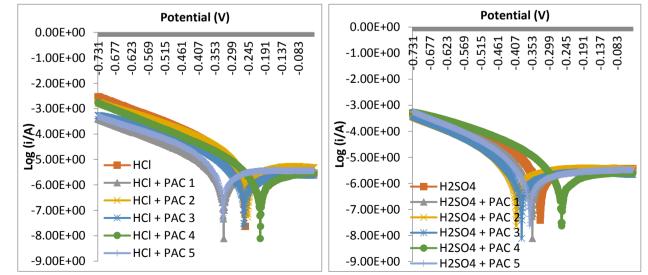
When iron corrodes, the rate is usually controlled by the cathodic reaction. There are several different cathodic reactions that are frequently encountered in metallic corrosion. The most common are:

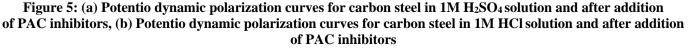
Hydrogen evolution  $2H^+ + 2e^- \longrightarrow H_2$ Oxygen reduction (acid solution)  $O_2 + 4 H^+ + 4e^- \longrightarrow 2H_2O$ Oxygen reduction (neutral or basic solution)  $O_2 + 4H_2O + 4e^- \longrightarrow 4OH^-$ Metal ion reduction  $M^{3+} + e^- \longrightarrow M^{2+}$ Metal deposition  $M^+ + e^- \longrightarrow M$ 

Hydrogen evolution is a common cathodic reaction since acidic media are frequently encountered. Oxygen reduction is very common, since any aqueous solution in contact with air is capable of reducing this reaction. Metal ion reduction and metal deposition are less common. All the above reactions are consuming electrons.

Since the anodic and cathodic reactions occurring during corrosion are mutually dependent, it is possible to reduce corrosion by reducing the rates of either reaction. So, if the surface of the metal is coated with paint or other conducting film, the rates of both anodic and cathodic reactions will be greatly reduced and corrosion will be retarded. The corrosion behaviour of metals and thus the corrosioninhibiting processes depend greatly on the anion composition of the electrolyte.

The values of electrochemical parameters i.e. corrosion current density ( $i_{corr}$ ), corrosion potential (Ecorr), Tafel slope ( $\beta c$ ) and inhibitor efficiency (IET, %) obtained as functions are measured.





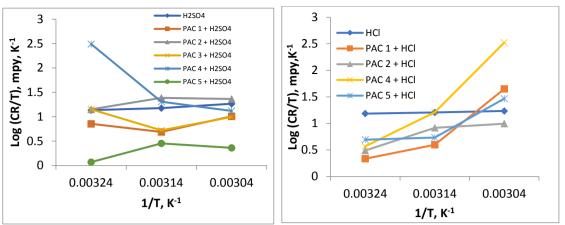


Figure 6: (a) log (corrosion rate/T) – (1/T) curves for dissolution in 1M H<sub>2</sub>SO<sub>4</sub> in absence and presence of PAC (1-5) absence and presence of inhibitor, (b) log (corrosion rate/T) – (1/T) curves for dissolution in 1M HCl in absence and presence of PAC (1-5) absence and presence of inhibitor

**Kinetic-thermodynamic corrosion parameters:** The effect of temperature  $(28^{\circ}C, 35^{\circ}C \text{ and } 45^{\circ}C)$  on the corrosion rate of iron in 1M HCl and H<sub>2</sub>SO<sub>4</sub> at different concentrations of inhibitors was studied using weight loss measurements. Plots of log k (corrosion rate) against 1/T (Figure 6), for iron dissolution at different concentrations of inhibitors gave straight lines. The values of the slopes obtained at different temperatures permit the calculation of Arrhenius activation energy (Ea\*). Activation parameters for corrosion of iron in 1M HCl and 1M H<sub>2</sub>SO<sub>4</sub> were calculated from Arrhenius type plot:

k=A exp (-Ea\*/RT)

and transition state type equation:

k=RT/Nh exp ( $\Delta$ S\*/R) exp ( $-\Delta$ H\*/RT)

The almost similar values of  $\Delta Ea^*$  suggested that the inhibitors are similar in the mechanism action and the order of the efficiency may be related with the pre-exponential factor A in equation (not shown).

The presence of investigated derivatives increases the activation energy of iron indicating strong adsorption of the inhibitor molecules on the metal surface. The presence of these additives induces energy barrier for the corrosion reaction and this barrier increases by increasing the additive concentration. The values of  $\Delta$ H\* reported are positive. The positive sign of the enthalpy reflects the endothermic nature of Fe dissolution process.

Also, the values of entropy of activation are negative. The negative values of entropy imply that the activated complex in the rate determining step represents an association rather than dissociation step, meaning that a decrease in disordering takes place on going from reactants to activated complex. A decrease in inhibition efficiency with rise in temperature suggests a possible desorption of some adsorbed inhibitor molecules from the metal surface at higher temperatures. Such behaviour indicates that inhibitor molecules were physically adsorbed on the metal surface.

### Conclusion

The PAC (1-5) inhibitors were synthesized in Schiff base mechanism by using eco-friendly microwave assisted method. All the PAC (1-5) inhibitors structures were characterized by using elemental analysis, IR, <sup>1</sup>H NMR and <sup>13</sup>C NMR. The inhibition efficiency of compounds PAC (1-5) was done by using weight loss method on 1M solution of HCl and H<sub>2</sub>SO<sub>4</sub>. The inhibition efficiency of the synthesized PAC (1-5) inhibitors increases with increase in inhibitor concentration and increase in temperature on 1M HCl and H<sub>2</sub>SO<sub>4</sub> medium.

The PAC (1-5) inhibitors obey Langumuir adsorption isotherm and in the kinetic study, the mechanism is an endothermic one and Tafel polarization plot indicates the PAC (1-5) inhibitors behave mixed type.

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